

# Application of Expert systems to WWTPs in CSC

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# Outline

- 1. Introduction**
- 2. Expert system in Biological WWTP**
- 3. Expert system in Industrial WWTP**
- 4. Summary**

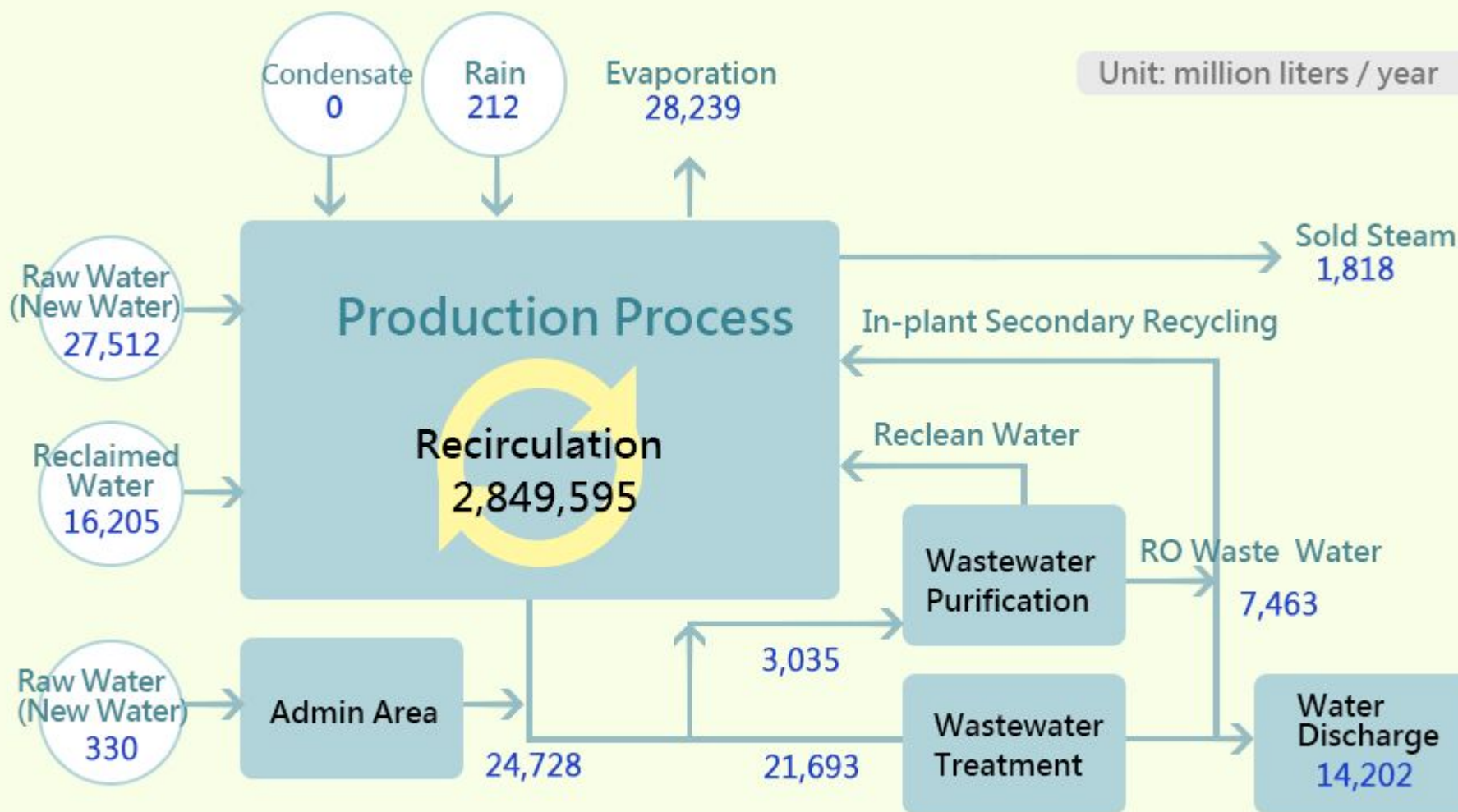


# 1.1 Introduction of CSC

- 1) **China Steel Corporation (CSC)**, located at Kaohsiung, Taiwan, was founded in December 1971.
- 2) It is the largest steel company in Taiwan with annual production (in terms of crude steel) around **10 million tons**.
- 3) The **domestic market** takes roughly **65%** of CSC's production and the exports take **35%**. The major export destinations are Mainland China, Japan, and Southeast Asia.

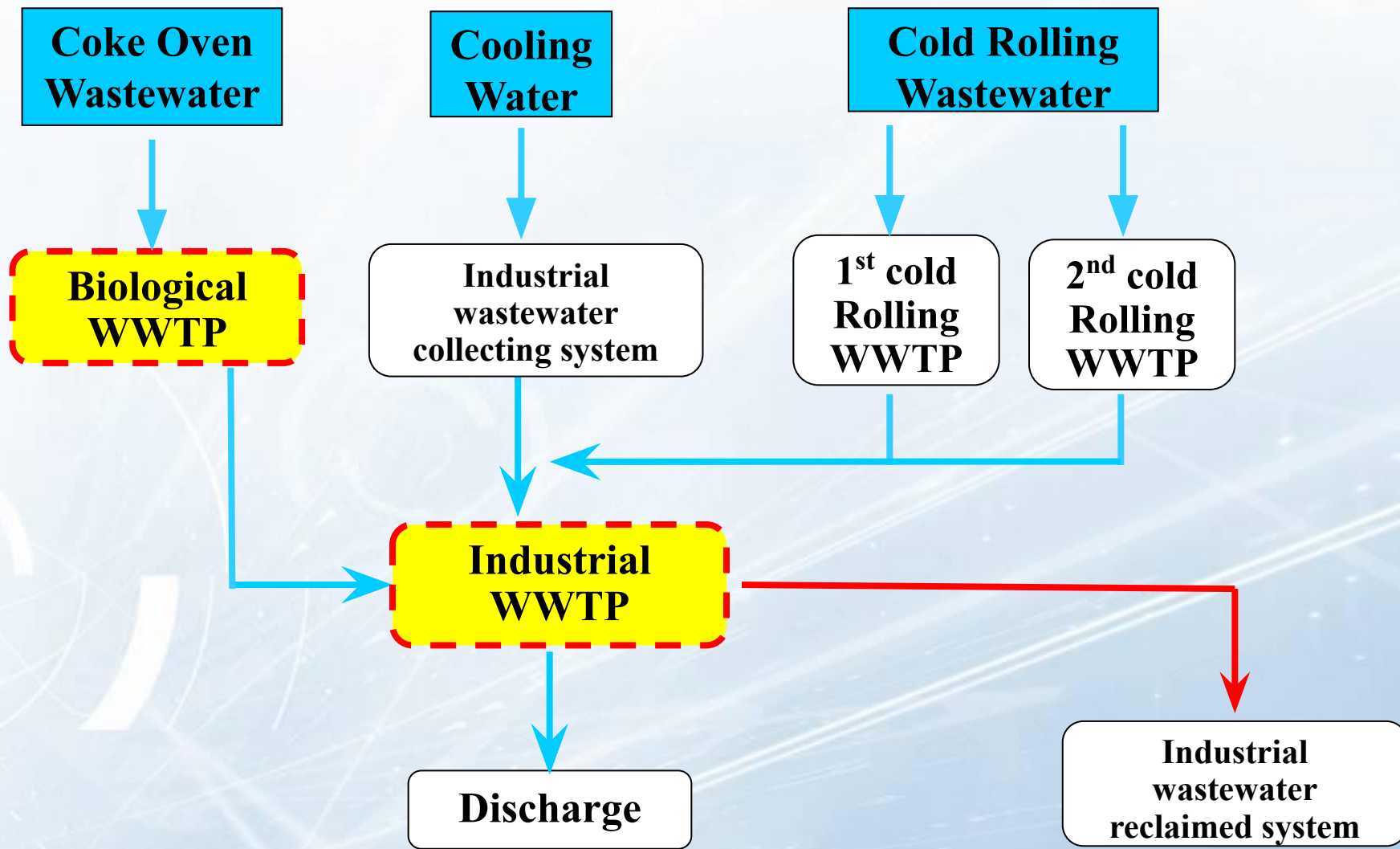


# 1.2 Water balance in CSC



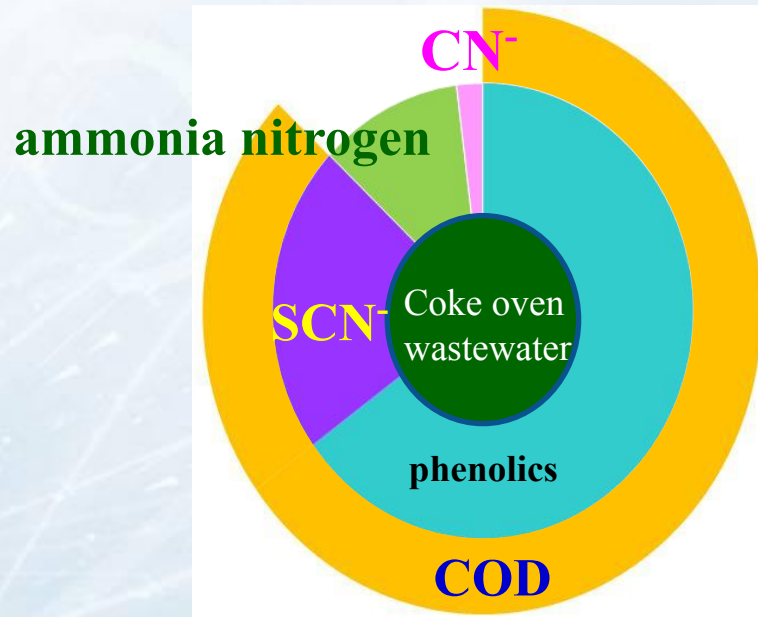
Note: The reclaimed water and tap water mentioned above are both fresh water.

# 1.3 Wastewater treatment in CSC



## 2.1 Composition of Coke Oven Wastewater

- 1) Coke oven wastewater contains **80%** of the **COD** and **90%** of the **ammonia nitrogen** produced from the entire CSC plant.
- 2) The composition of coke oven wastewater is complicated and mainly includes **phenolics**, **thiocyanate**, **ammonia nitrogen**, and **cyanide**.



## 2.2 Problems and difficulties

Eutrophication caused by ammonia nitrogen



Biological WWTP used to only treat COD  
Ammonia nitrogen of effluent: **400~500mg/L**

↓  
**Reconstruction**  
↓

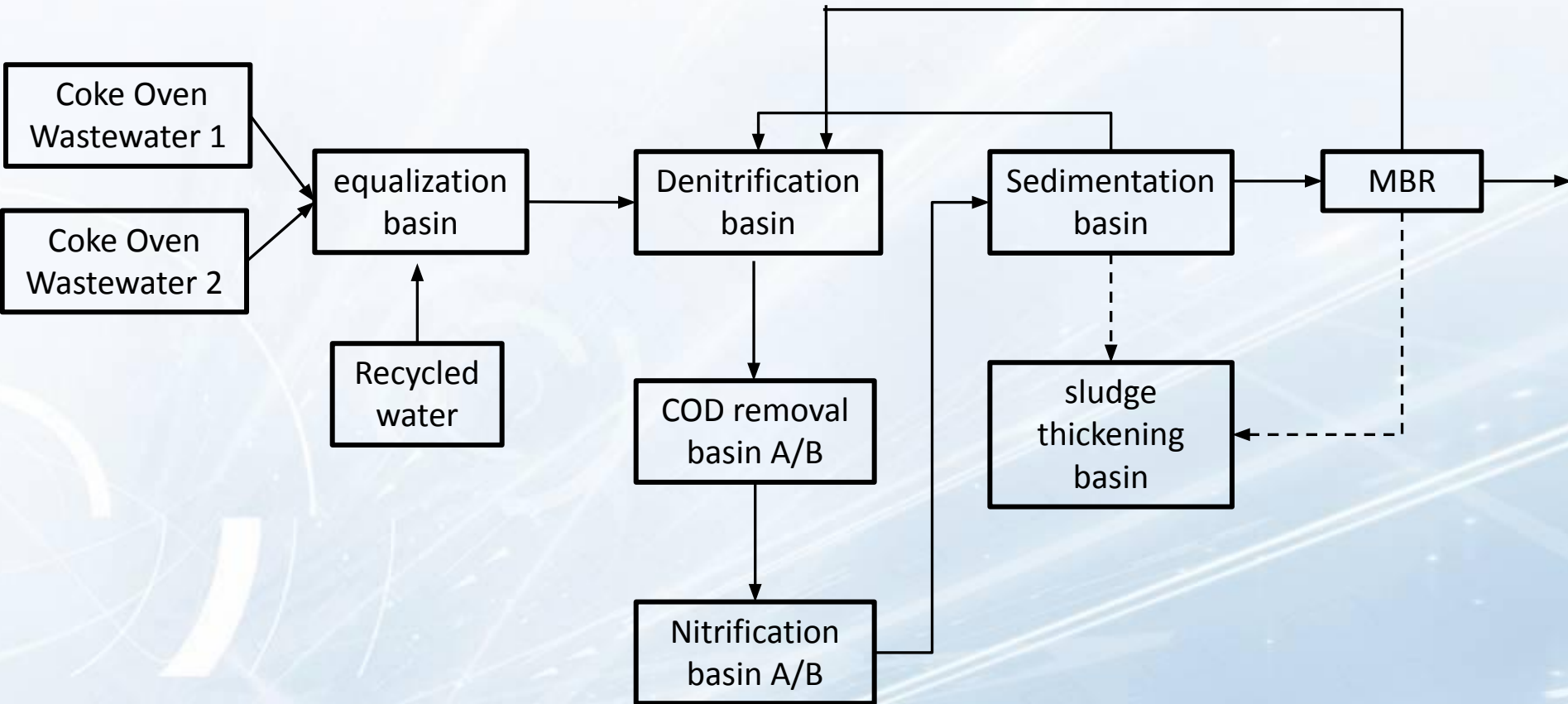
Ammonia nitrogen of effluent: **<10 mg/L**

**Ammonia nitrogen** of discharge water needs **<20 mg/L** before 2017.11.01

Reconstructed in the original WWTP

- HRT is only **38 hrs**
- the system is more vulnerable to the fluctuations in the coke oven wastewater
- the residual **organic compounds** inhibit the nitrification reaction

## 2.3 Biological WWTP treatment process after reconstruction





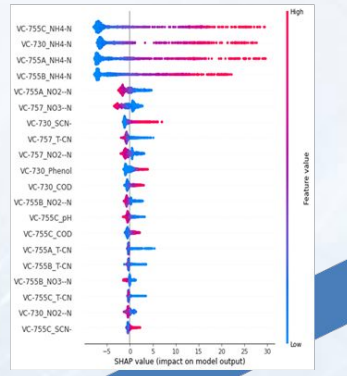
# 2.4 Flowchart to build a expert system



data collection

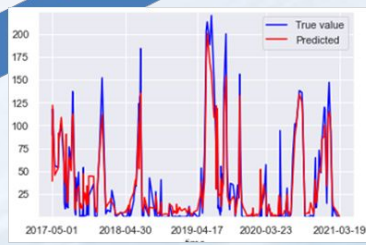
CHL2	pH	Cond	Phenol	NH <sub>4</sub> -N	T-CN	SCN	Color	S.S.	VSS	VSS/SS	COD	PO <sub>4</sub>	SO <sub>4</sub>
mg/L		mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	mg/L	%	mg/L	mg/L	mg/L
0001	7.2	200	0.05	1.0	0.5	0.1	10	100	100	100	100	100	100
0002	7.3	210	0.06	1.1	0.6	0.1	11	110	110	110	110	110	110
0003	7.4	220	0.07	1.2	0.7	0.1	12	120	120	120	120	120	120
0004	7.5	230	0.08	1.3	0.8	0.1	13	130	130	130	130	130	130
0005	7.6	240	0.09	1.4	0.9	0.1	14	140	140	140	140	140	140
0006	7.7	250	0.10	1.5	1.0	0.1	15	150	150	150	150	150	150
0007	7.8	260	0.11	1.6	1.1	0.1	16	160	160	160	160	160	160
0008	7.9	270	0.12	1.7	1.2	0.1	17	170	170	170	170	170	170
0009	8.0	280	0.13	1.8	1.3	0.1	18	180	180	180	180	180	180
0010	8.1	290	0.14	1.9	1.4	0.1	19	190	190	190	190	190	190
0011	8.2	300	0.15	2.0	1.5	0.1	20	200	200	200	200	200	200
0012	8.3	310	0.16	2.1	1.6	0.1	21	210	210	210	210	210	210
0013	8.4	320	0.17	2.2	1.7	0.1	22	220	220	220	220	220	220
0014	8.5	330	0.18	2.3	1.8	0.1	23	230	230	230	230	230	230
0015	8.6	340	0.19	2.4	1.9	0.1	24	240	240	240	240	240	240
0016	8.7	350	0.20	2.5	2.0	0.1	25	250	250	250	250	250	250
0017	8.8	360	0.21	2.6	2.1	0.1	26	260	260	260	260	260	260
0018	8.9	370	0.22	2.7	2.2	0.1	27	270	270	270	270	270	270
0019	9.0	380	0.23	2.8	2.3	0.1	28	280	280	280	280	280	280
0020	9.1	390	0.24	2.9	2.4	0.1	29	290	290	290	290	290	290
0021	9.2	400	0.25	3.0	2.5	0.1	30	300	300	300	300	300	300

data collection



ranking of variable factors

algorithm testing



suitable operating strategies

	Old values	Suggest values	Old values	Suggest values	
1. VC-730_NH4-N	35.60	26.15	6. VC-730_Phenol	0.06	0.01
2. VC-755B_NH4-N	0.40	0.40	7. VC-730_SCN-CN	3.28	2.85
3. VC-755C_NH4-N	25.90	17.52	8. VC-757_T-CN	2.24	2.21
4. VC-755A_NH4-N	1.70	1.70	9. VC-757_NO2--N	2.44	2.65
5. VC-757_NO3--N	28.80	27.33	10. VC-755B_NO3--N	36.40	36.14
Old values Suggest values					
11. VC-755C_pH	7.94	7.94			
12. VC-755C_SCN-CN	21.60	21.28			
13. VC-757_COD	123.00	122.53			
14. VC-755B_NO2--N	6.78	6.89			
15. VC-755C_COD	469.00	467.42			

Internal control:  
ammonium nitrogen  
< 10 mg/L

## 2.5 Evaluate and screen relative parameters

Monitoring target	Parameters assayed in lab
Coke oven wastewater1	pH, conductivity, phenol, ammonia, $\text{CN}^-$ , $\text{SCN}^-$ , COD
Coke oven wastewater2	pH, conductivity, phenol, ammonia, $\text{CN}^-$ , $\text{SCN}^-$ , COD
equalization basin	pH, conductivity, phenol, ammonia, $\text{CN}^-$ , $\text{SCN}^-$ , COD
COD removal basin	pH, conductivity, phenol, ammonia, $\text{CN}^-$ , $\text{SCN}^-$ , COD, S.S., $\text{NO}_2^-$ , $\text{NO}_3^-$
Nitrification basin A	pH, ammonia, $\text{CN}^-$ , $\text{SCN}^-$ , S.S., COD, $\text{NO}_2^-$ , $\text{NO}_3^-$
Nitrification basin B	pH, ammonia, $\text{CN}^-$ , $\text{SCN}^-$ , S.S., COD, $\text{NO}_2^-$ , $\text{NO}_3^-$
Denitrification basin	pH, conductivity, ammonia, $\text{CN}^-$ , S.S., COD, $\text{NO}_2^-$ , $\text{NO}_3^-$
Effluent	pH, conductivity, ammonia, $\text{CN}^-$ , COD, $\text{NO}_2^-$ , $\text{NO}_3^-$

Monitoring target	Parameters monitored online
equalization basin	Temperature
COD removal basin	pH, temperature, pure oxygen flow rate
Nitrification basin A	temperature, dissolved oxygen, pure oxygen flow rate
Nitrification basin B	temperature, dissolved oxygen, pure oxygen flow rate
Denitrification	temperature, dissolved oxygen, pure oxygen flow rate

**63** factors which are assayed daily in **lab** and **15** factors which are monitored by **online** detectors were selected

# 2.6 Inventory of all monitoring parameters and controlling strategies

## Monitoring parameters

item	monitoring frequency
15 online parameters	continuously
63 parameters which are assayed daily in lab	Mon~Fri
S.S.; VSS	1 times/week

## Controlling strategies:

issue	Controlling strategy
CN <sup>-</sup> of influent >10mg/L	Add <b>FeSO<sub>4</sub></b> into the basins to form Prussian blue <b>Fe<sub>4</sub>[Fe(CN)<sub>6</sub>]<sub>3</sub></b> to remove toxicity
metabolism of biomass decreases	Add <b>nutrient salts</b> and <b>vitamins</b> to stimulate metabolism
decrease of biomass	Implant sludge from other biological WWTP

S.S.: suspended solids; VSS: volatile suspended solids

## 2.7 model selection and testing

	(1)	(2)	(3-1)	(3-2)
data source	lab	online	lab + online	lab + online
parameters	63	15	63+15	63+15
data amount	1240	1240 1 data set /day	34201 1 data set/hr	1240 1 data set/day
Training $R^2$	0.92	0.89	0.95	0.93
Testing $R^2$	0.91	0.39	0.95	0.9

1. (3-1) seems better than (1). However it's caused by data processing and the lab data is used too repeatedly  **overfitting** phenomenon.
2. **SHapley Additive exPlanations** analysis showed that the correlation between 15 online parameters and ammonia nitrogen in the effluent is relatively low.

**(1) was chosen and the model is built using XGBoosting algorithm**



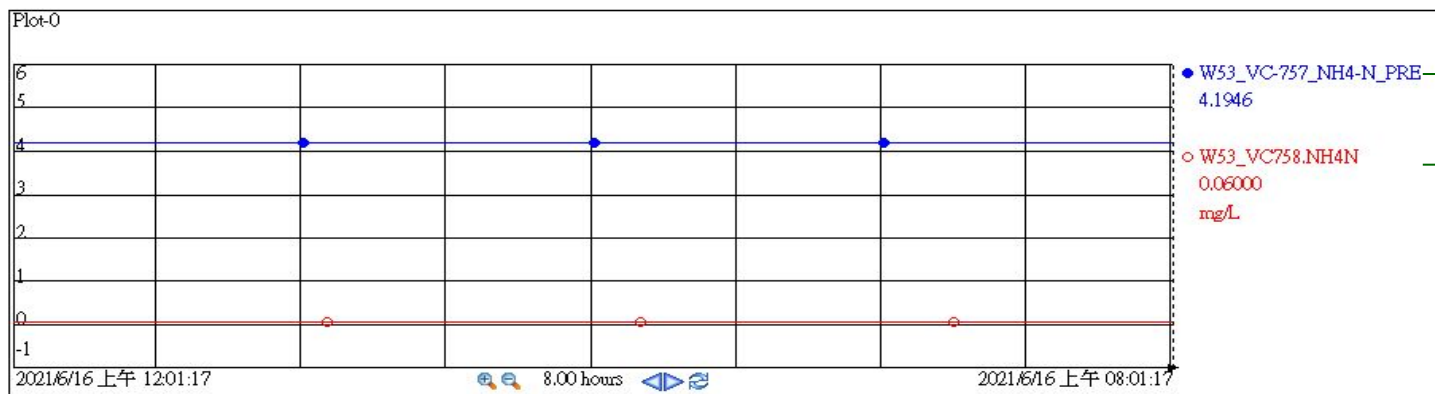
## 2.8 Importance of parameters analysis

Ranking	parameter	Importance
1	$\text{NH}_3\text{-N}$ of Denitrification basin	0.172
2	$\text{NH}_3\text{-N}$ of COD removal basin	0.155
3	$\text{NH}_3\text{-N}$ of Nitrification basin A	0.153
4	$\text{NH}_3^-$ of Nitrification B basin	0.145
5	$\text{NO}_2^-$ of Nitrification A basin	0.030
6	$\text{NO}_3^-$ of effluent	0.028
7	$\text{SCN}^-$ of COD removal basin	0.024
8	$\text{CN}^-$ of influent	0.019
9	$\text{NO}_2^-$ of effluent	0.019
10	Phenol of COD removal basin	0.016

⋮

The importance of parameters to affect the ammonia concentration in the are ranked using SHapley Additive exPlanations

# 2.9 Results to Operators



→ Predicted  
NH<sub>3</sub>-N

→ Actual  
NH<sub>3</sub>-N

Detected number in lab

← Old values

Suggest values

Old values

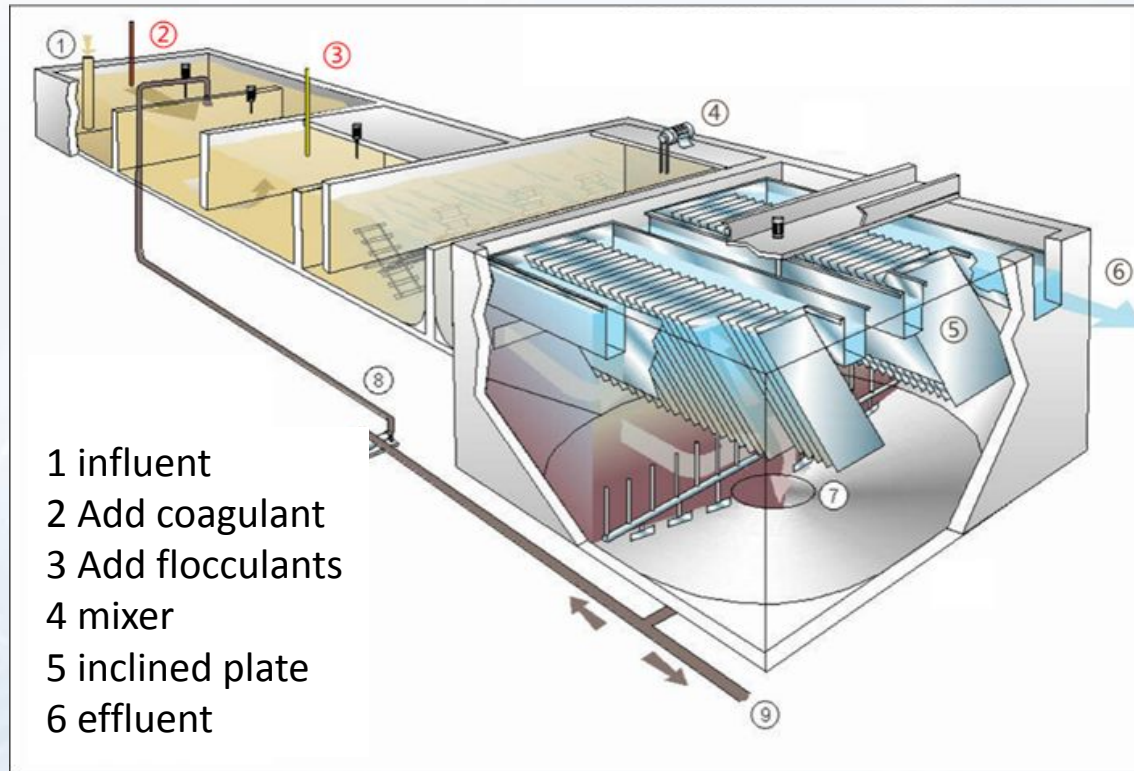
Suggest values

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**Target: NH<sub>3</sub>-N < 10 mg/L  
in effluent**

**The number of days that the ammonia nitrogen in effluent exceeding the internal control has dropped significantly to 1.3%**

# 3.1. Process of industrial WWTP



**Coagulation, flocculation, and sedimentation are used to remove the suspended solids and turbidity.**

## 3.2 Problems and difficulties

- 1) The sedimentation depends on the **size of the flocs**. The human eye is used to judge and the **chemical adding dosage** is base on operator's **experience**.
- 2) **Excess amount** of chemicals are usually added in order to ensure water quality of the discharge water. There will be a waste in **chemical dosing** and **sludge handling** fee.



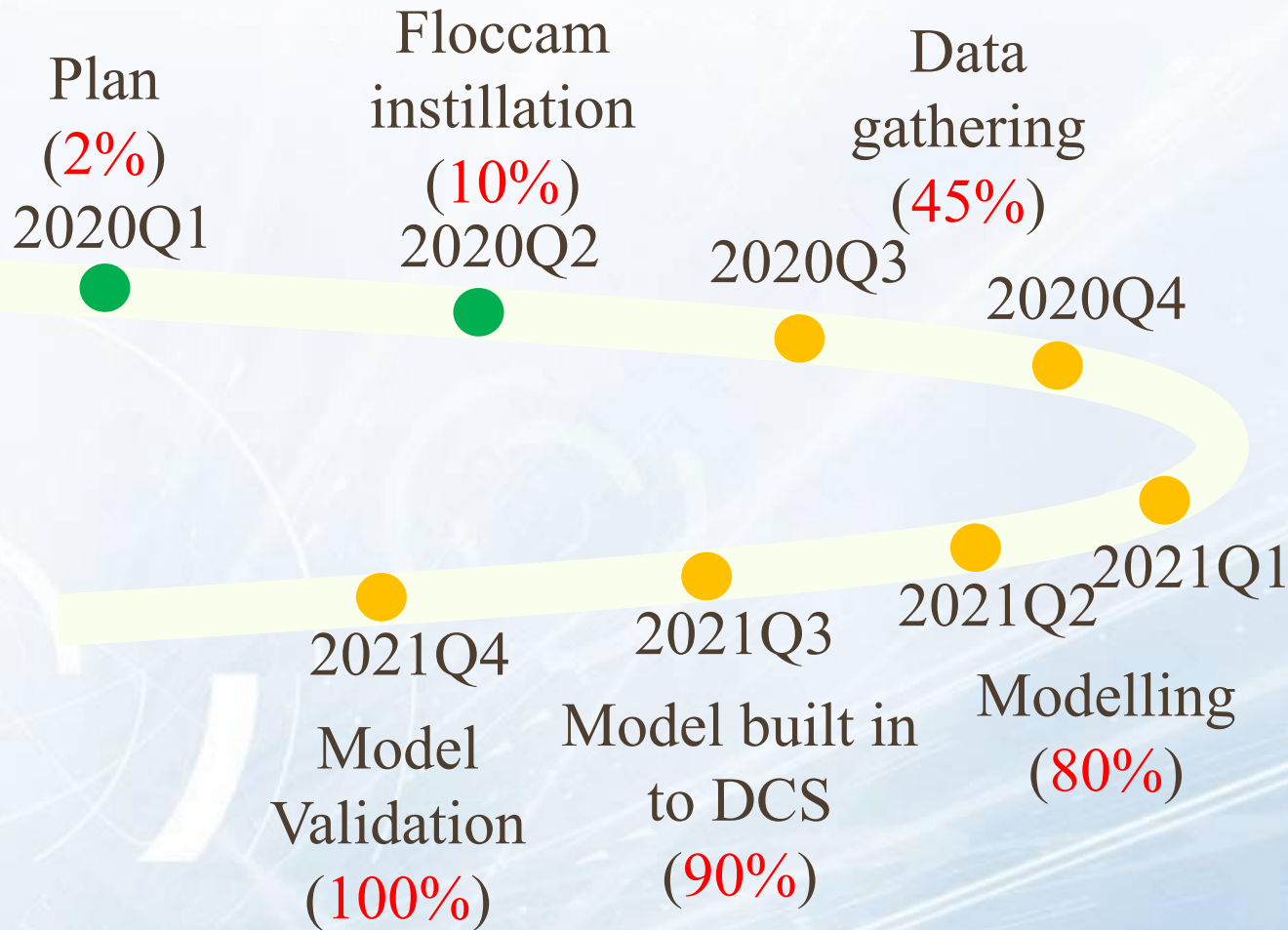
**Insufficient dosage  
No flocs formation**



**Optimal dosage  
flocs formation**



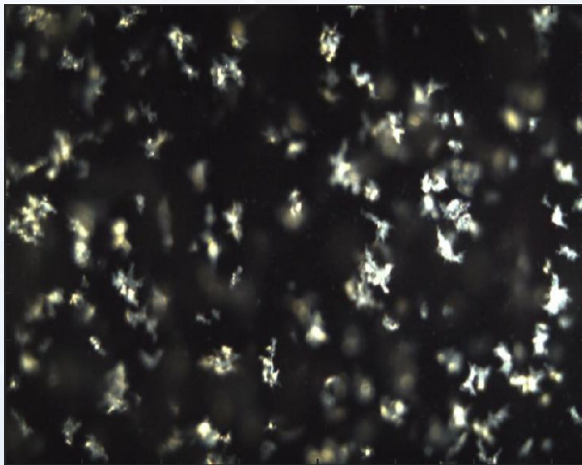
# 3.3 Development approach



**Target: optimize the chemical dosing and reduce the fee to at least 3%**

# 3.4 Floc capture and data collection

- 1) **Floccam instillation:** flocs are captured and the images are converted to **20** quantitative parameters.
- 2) **Data Collection:** floccam data together with **10** other factors, are all monitored online and the **AVEVA PI (Plant Information) System** was used to collect and store the data.



Flocs captured by floccam

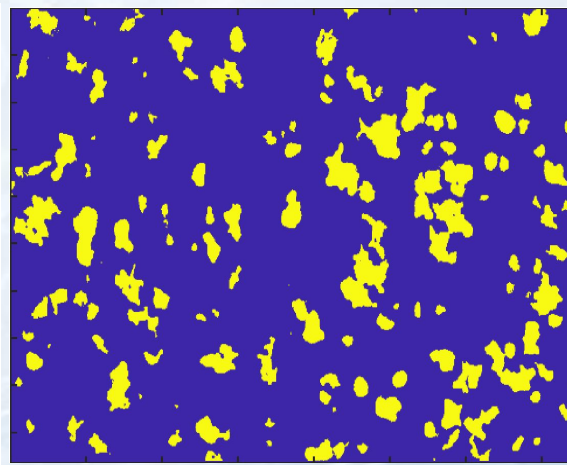


Image analysis-  
Floc and background

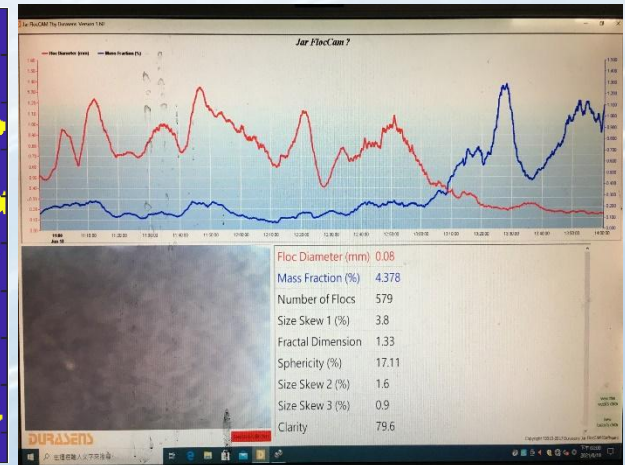
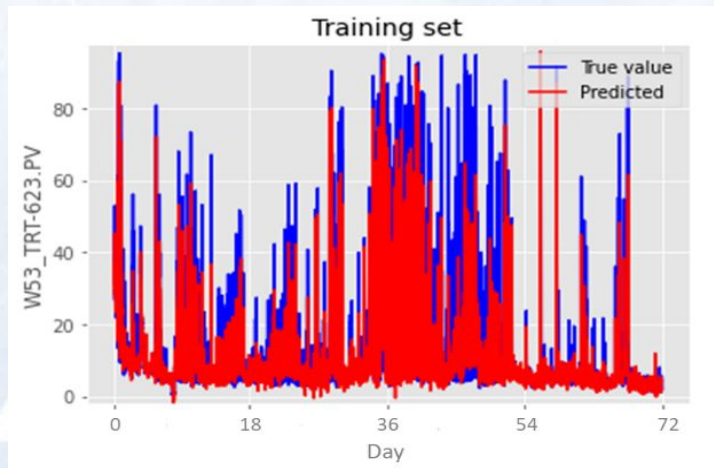


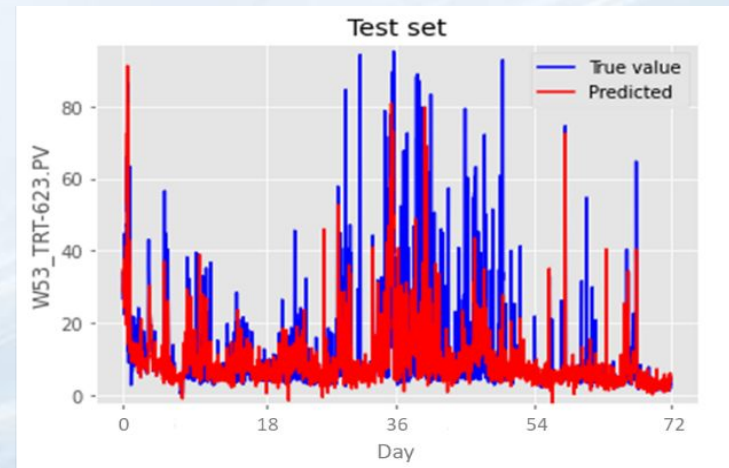
Image converts to  
quantitative data

# 3.5 Data selection and modelling

- 1) Data source: **20** variables from **floccam** and other **10** variables, including chemical dosing concentration, pH, and water volume flow rate of influent.
- 2) Target: **S.S. of effluent < 30 mg/L**
- 3) Data gathering frequency is **every 5 mins** and the HRT is taken into account that the model is set to predict the result **in 25 minutes** later.
- 4) Testing algorithm: random forest, **XGBoosting**, and deep learning



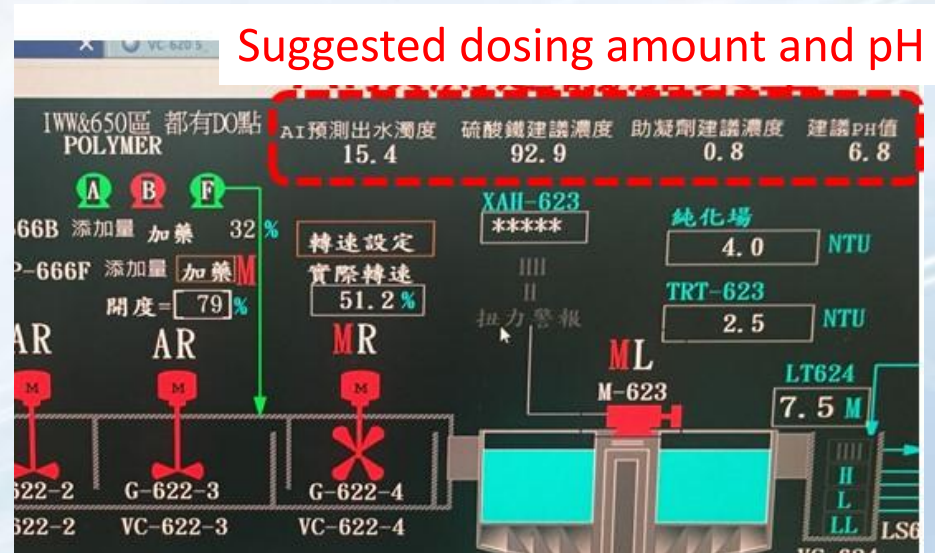
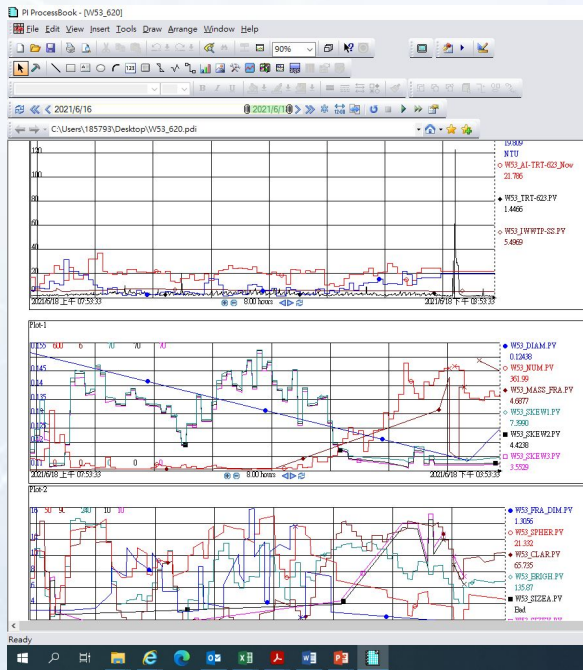
Training



Testing

# 3.6 Result shown on DCS

- 1) SHapley Additive exPlanations is used to analyze the importance of each variables
- 2) The suggested **chemical dosing concentration** and **pH** were calculated, exported from PI system, and shown on **DCS**



## 3.7 Benefit assessment

- Better quality of Effluent:** The average **S.S concentration** is **5.35** and the maximum is 13, which is lower than the **30 mg/L** effluent standard.
- Save dosing fee:** the **coagulant** and the **floculant** used per unit of wastewater was decreased by **4.1%** and **22.4%**, respectively. The total chemical dosing fee was decreased by **4.8%** which is meeting the initial **3% target**.

	coagulant		floculant		Total dosing fee		Water quality	
	dosage	Difference %	dosage	Difference %	dosage	Difference %	S.S. average	S.S Max
Before	0.161		0.000399		0.675		16.9	24
After	0.154	-4.1	0.000309	-22.4	0.643	-4.8	5.35	13

# 4.1 Summary

## Expert system in Biological WWTP

- **Model:** Lab data and **XGBoost** were used
  - **Predict and warning:** predict **NH<sub>3</sub>-N** value in effluent
  - **Optimal operation:** pick up the key factors that affect the **NH<sub>3</sub>-N** in the effluent and give suggested value of the key factors.
- The number of days that the **NH<sub>3</sub>-N** exceeding the **internal control** has dropped significantly to **1.3%**

## Expert system in Industrial WWTP

- **Model:** 20 Floccam data, 10 online data, and **Xgboost** were used
  - **Predict and warning:** predict **S.S.** value in effluent **25 minutes** later
  - **Optimal Operation:** give suggested **chemical dosing concentration** and **pH**
- The total **chemical dosing fee** was decreased by **4.8%** which is meeting the initial **3% target**.

## 4.2 Future Plan

1. The data of both WWTP will be continuously collected, accumulated and stored in **the AVEVA PI System**.
2. The expert systems of both WWTP would be fixed and modified **every 6 months**.
3. The research team and operators would have regular communication and discussion to improve both systems.



# *Thank You*

